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Thermodynamic Description of Aqueous Species in the System Cu–Ag–Au–S–O–H at Temperatures of 0–600°C and Pressures of 1–3000 Bar

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INTRODUCTION

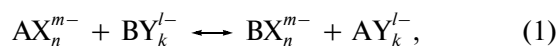
Understanding the processes responsible for the mobilization, transport, and deposition of the ore-forming Ag–Au–Au triad is largely underlain by the availability of reliable thermodynamic information on the components of this system. Experimental data accumulated so far on the behavior of these elements in hydrothermal solutions are unsystematic and often inconsistent. The thermodynamic reviews [1, 2] published in the late 1990s have not eliminated this problem, because the parameters of complex species reported therein were based mostly on empirical correlations based on the “free” Cu⁺ and Au⁺ ions, whose properties were determined unreliably. This was the reason why we attempted, in 2001, to generalize and process experimental information accumulated by that time on the stability constants of chloride, hydrosulfide, and hydro-complexes of Ag(I), Cu(I), and Au(I) in hydrothermal conditions. The thermodynamic summary on this basis for the system Ag(I)–Cu(I)–Au(I)–S(II)–Cl–O–H was published in [3]. Experimental data were recently published on the stability of Cu and Au hydrosulfide complexes at low temperatures [4, 5], and new data were obtained on Au and Ag behavior in hydrothermal sulfide solutions [6–8]. Our research was focused on the correction of thermodynamic constants for Cu, Ag, and Au hydrosulfide complexes with regard to lately obtained experimental data.

METHODS

The behavior of solute components at high temperatures and pressures can be predicted with the use of the Helgeson–Kirkham–Flowers (HKF) equation of state [9–11], which is currently widely applied for this purpose. This equation makes it possible to accurately enough describe the limiting thermodynamic properties of aqueous solutions within broad ranges of temperatures (25–1000°C) and pressures (1–6000 bar). In order to comprehensively describe the thermodynamic properties of a

component of aqueous solution, one should know its standard thermodynamic properties ($\Delta_f G_{298}^\circ$ and S_{298}°), Born parameter (ω), and six parameters determining the temperature and pressure dependences for the partial volume (a_1, \dots, a_4) and heat capacity (c_1, c_2). Empirical relations suggested in [12], and referred here to as *inner correlations* between HKF parameters, make it possible to “reproduce” the set of HKF parameters of a species if its $C_{p,298}$, V_{298} , and ω are known.

In the absence of reliable experimental data, the method of *isocoulombic reactions* [13] can be applied. It was demonstrated [14, 15] that, for exchange reactions with the participation of solute components



the temperature and pressure dependences of the equilibrium constant can be estimated ignoring the changes in the heat capacity ($\Delta_r C_p \approx 0$) and molar volume ($\Delta_r V \approx 0$) of the reaction.

Where not specified otherwise below, the values of thermodynamic properties of pure phases (*native silver*, *acanthite/argentite* (Ag₂S), and H₂, O₂, and H₂S gases), “simple” ions (Na⁺, Cl[−], HS[−], and OH[−]), and ion pairs (NaCl_{aq} and NaOH_{aq}) were borrowed from the SUPCRT92 thermodynamic database [16] and its extensions [1, 2] without any revisions and amendments, and HKF parameters of HCl_{aq} were compiled from [17].

The thermodynamic properties of aqueous hydrogen sulfide H₂S_{aq} were calculated by a newly obtained equation of state for neutral aqueous species [18]. The application of this equation makes it possible to eliminate errors inherent to the HKF model when applied to dissolved gases in near- and supercritical regions of H₂O [19]. As an illustration of this, in Fig. 1, we compare experimental values for the partial molar volume of aqueous hydrogen sulfide with the analogous values calculated by the HKF model (dashed lines) and equation from [18] (solid lines).

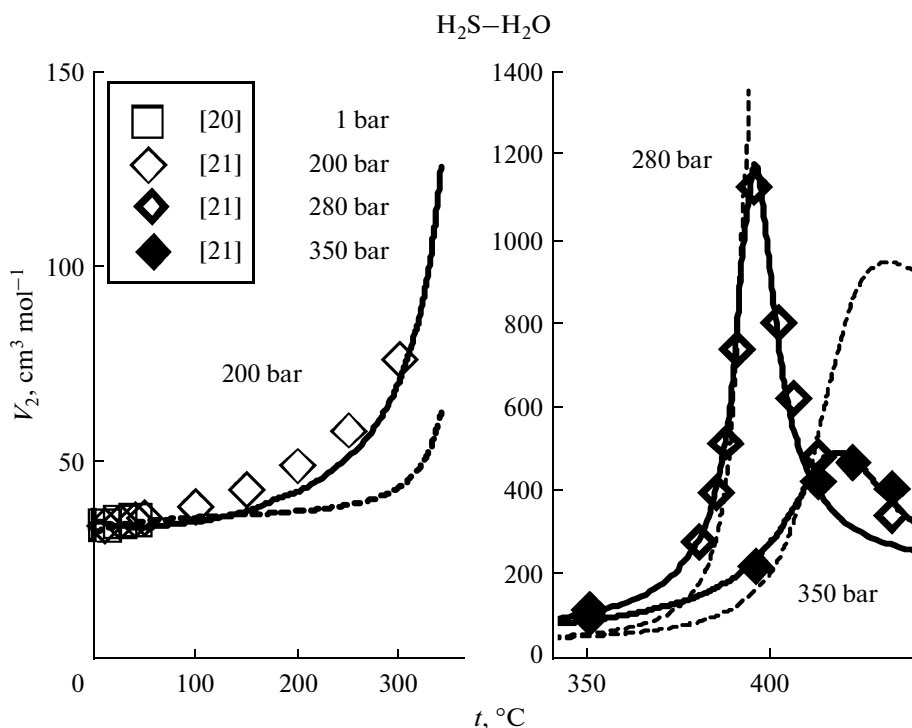


Fig. 1. Temperature dependence of the partial volume of dissolved H_2S at pressures of 1, 200, 280, and 350 bar. Lines represent calculation results: dashed lines—HKF model and solid line—equation of state [18].

It can be readily seen that the application of the newly obtained equation of state significantly improves the accuracy of the description for $\text{H}_2\text{S}_{\text{aq}}$ in the near- and supercritical regions. At the same time, when a temperature dependence is derived for Henry constant of aqueous $\text{H}_2\text{S}_{\text{aq}}$ can be reproduced by use of the proposed equation of state within the experimental error in subcritical (0–360°C, water saturation pressure) region and enables oneself reasonable description of the $\text{H}_2\text{S}_{\text{aq}}$ in the supercritical region [22] as well (Fig. 2).

The parameters of the equation of state for solute $\text{H}_2\text{S}_{\text{aq}}$ assumed herein are listed in Table 1. They are somewhat different from those reported in [18] due to other optimization conditions: we took into account the statistical weight of the data [26] at 250–350°C. The values of the standard chemical potential of $\text{H}_2\text{S}_{\text{aq}}$ calculated with the assumed values of the empirical parameters of the equation of state (Table 1, ξ , a , and b) are presented in Table 2.

The HKF parameters for solute components were fitted with the use of the UT-HEL computer program [27], which enables one to minimize discrepancies between experimentally determined and calculated values for the Gibbs function of a component by optimizing the values of its standard chemical potential μ_{298} , entropy S_{298} , and all seven coefficients of the HKF equation: $a_1, \dots, a_4, c_1, c_2$, and ω .

OPTIMIZATION RESULTS

As was mentioned above, the internally consistent thermodynamic database for the system Cu–Ag–Au–S–O–H presented herein (Tables 1–2) is based on the recently published thermodynamic database [3], with certain corrections introduced into it with regard to experimental results published in 2001–2006 [4–8]. We

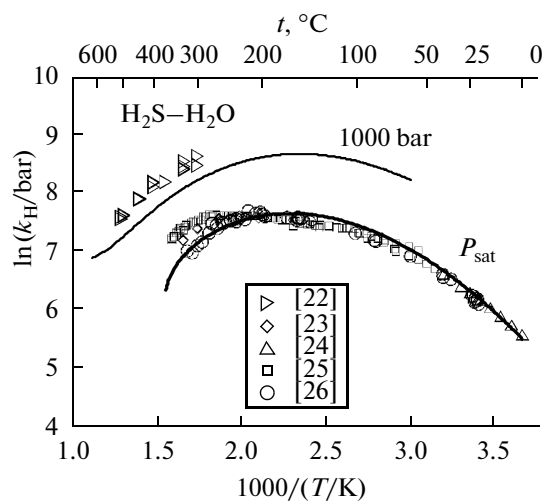


Fig. 2. Temperature dependence of the Henry constant of H_2S at various pressures. Symbols—experimental results and lines—calculation using equation of state [18] with parameters from Table 1.

Table 1. Thermodynamic parameters of the equation of state [18] assumed herein for solute hydrogen sulfide $\text{H}_2\text{S}_{\text{aq}}$

| $\Delta_f G_{298}^{\circ a}$ | $\Delta_f H_{298}^{\circ a}$ | $S_{298}^{\circ b}$ | V_{298}^c | $C_{p, 298}^b$ | ξ | a^d | b^e |
|------------------------------|------------------------------|---------------------|-------------|----------------|---------|----------|---------|
| -6652 | -9402 | 28.916 | 34.9 | 52.64 | -0.2017 | -12.8031 | 13.5396 |

Note: a cal mol $^{-1}$; b cal mol $^{-1}$ K $^{-1}$; c cm 3 mol $^{-1}$; d cm 3 g $^{-1}$; e cm 3 K $^{0.5}$ g $^{-1}$.

Table 2. Chemical potentials of aqueous $\text{H}_2\text{S}_{\text{aq}}$ at various pressures and temperatures $\mu_{p,T}^0$ (cal mol $^{-1}$) standardized according to the HKF equation of state; P_s corresponds to the H_2O vapor saturation pressure

| Temperature, °C | Pressure, bar | | | | | |
|-----------------|---------------|--------|--------|--------|--------|--------|
| | P_s | 500 | 1000 | 1500 | 2000 | 3000 |
| 0 | -5991 | -5567 | -5167 | -4787 | -4423 | -3735 |
| 25 | -6652 | -6246 | -5859 | -5488 | -5130 | -4450 |
| 50 | -7426 | -7024 | -6640 | -6271 | -5915 | -5236 |
| 100 | -9231 | -8816 | -8423 | -8047 | -7685 | -6995 |
| 150 | -11312 | -10868 | -10452 | -10059 | -9683 | -8971 |
| 200 | -13618 | -13133 | -12681 | -12262 | -11867 | -11125 |
| 250 | -16125 | -15579 | -15077 | -14624 | -14203 | -13426 |
| 300 | -18831 | -18192 | -17613 | -17117 | -16666 | -15849 |
| 350 | -21831 | -20972 | -20270 | -19718 | -19232 | -18371 |
| 400 | | -23952 | -23030 | -22406 | -21881 | -20975 |
| 450 | | -27186 | -25869 | -25161 | -24595 | -23644 |
| 500 | | -30258 | -28756 | -27961 | -27355 | -26364 |
| 550 | | -33060 | -31638 | -30784 | -30147 | -29123 |
| 600 | | -35815 | -34481 | -33612 | -32956 | -31912 |

have revised and recalculated the thermodynamic properties of four hydrosulfide complexes: $\text{Cu}(\text{HS})_2^-$, $\text{Ag}(\text{HS})_{\text{aq}}^-$, $\text{Au}(\text{HS})_{\text{aq}}^-$, and $\text{Au}(\text{HS})_2^-$.

$\text{Cu}(\text{HS})_2^-$. In the absence of reliable experimental data, the thermodynamic properties of this complex were evaluated in our earlier paper [3] for the reaction



on the basis of data in [28] for a temperature of 22°C and using the isocoulombic approach for the reaction of the participation of another chloride complex of Cu(I). The experimental data [4] recently obtained for the temperature interval of 35–95°C led to the revision of the entropy value of this complex. The optimization results obtained with the UT-HEL program are shown in Table 3, and the accuracy of the description is illustrated in Fig. 3a. Data in [34] on the solubility of Cu-bearing mineral associations at temperatures of 200–350°C recalculated to the $\text{Cu}(\text{HS})_2^-$ complex

exhibit systematic deviations (1.5–2 kcal mol $^{-1}$) and were rejected from the optimization procedure. It should be mentioned that the values of the entropy of the complex was significantly changed (by 10 cal mol $^{-1}$ K $^{-1}$) in comparison to the estimation [3] based on the isocoulombic reaction retaining the same value for $C_{p,298}$.

$\text{AgHS}_{\text{aq}}^-$. Ad hoc key [5] led us to suggest that the data [6, 35] on the solubility of crystalline silver sulfide at room temperature are overestimates. These researchers likely failed to completely preclude the oxidation of hydrogen sulfide and the possible occurrence of silver thiosulfate complexes. The Ag_2S solubility determined with the application of a radioactive tracer in [36, 37] is significantly lower than the values measured by other researchers and is likely devoid of this error. Because of this, the low-temperature data in [5, 6, 35, 38, 39] for temperatures lower than 100°C were rejected from the optimization procedure.

Table 3. Standard thermodynamic properties (298.15 K, 1 bar) and HKF parameters of aqueous species assumed herein

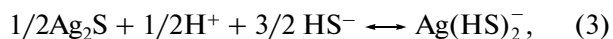
| Component | $\Delta_f G_{298}^{\circ a}$ | $\Delta_f H_{298}^{\circ a}$ | S_{298}^b | $C_{p, 298}^b$ | V_{298}^c | $a_1 \times 10^d$ | $a_2 \times 10^{-2 a}$ | a_3^e | $a_4 \times 10^{-4 f}$ | c_1^b | $c_2 \times 10^{-4 f}$ | $w \times 10^{-5 a}$ | Reference |
|----------------------------------|------------------------------|------------------------------|--------------------|------------------|-------------|---------------------|------------------------|---------------------|------------------------|-----------------------|------------------------|----------------------|-----------|
| HS ⁻ | 2860 | -3859 | 16.30 | -22.5 | 20.2 | 5.0119 | 4.9799 | 3.4765 | -2.9849 | 3.4200 | -6.2700 | 1.4410 | [16] |
| AgCl ₂ ⁻ | -51350 | -60092 | 49.78 | -16.6 | 37.1 | 7.1327 | 9.8065 | 1.8947 | -3.1844 | 4.8953 | -6.7789 | 0.6667 | [3] |
| AgHS _{aq} | 2314 ⁱ | 2722 | 34.77 ⁱ | 1.8 ⁱ | 24.5 | 5.1121 ^h | 4.7007 ^h | 3.9024 ^h | -2.9733 ^h | -36.0117 ^h | 18.6121 ^h | 0.0 | |
| Ag(HS) ₂ ⁻ | 287 | -6636 | 49.00 | 3.4 | 42.8 | 7.8651 | 11.4225 | 1.2604 | -3.2512 | 13.9576 | -2.3624 | 0.6367 | [3] |
| CuHS _{aq} | -3401 | 883 | 45.56 | -8.7 | 38.3 | 4.7896 | 3.9132 | 4.2119 | -2.9408 | 5.3754 | -3.3096 | 0.0 | [3] |
| Cu(HS) ₂ ⁻ | -5902 | -12725 | 47.09 ^j | -1.2 | 70.1 | 11.6490 | 20.6614 | -2.3710 | -3.6331 | 12.6022 | -3.2693 | 0.7794 | |
| AuCl ₂ ⁻ | -36795 | -46000 | 47.16 | -26.4 | 68.6 | 11.4774 | 20.2425 | -2.2063 | -3.6158 | 27.0677 | -22.440 | 0.8623 | [3] |
| AuHS _{aq} | 8344 ⁱ | 11032 | 50.86 ⁱ | 1.8 | 56.5 | 9.4965 | 15.4057 | -0.3052 | -3.1459 | -38.1356 ⁱ | 19.6524 ⁱ | 0.0 | |
| Au(HS) ₂ ⁻ | 3487 ⁱ | 4703 | 77.46 | 3.3 | 75.1 | 12.3373 | 22.3421 | 3.0317 | -3.7026 | -53.6010 | 31.4030 | 0.7673 | |

Note: ^a cal mol⁻¹; ^b cal mol⁻¹ K⁻¹; ^c cm³ mol⁻¹; ^d cal mol⁻¹ bar⁻¹; ^e cal K mol⁻¹ bar⁻¹; ^f cal K mol⁻¹. Methods used to determine the thermodynamic parameters of the complexes: ^h correlations between parameters of the HKF equation [12]; ⁱ least-squares method, UT-HEL program [27].

The thermodynamic parameters of AgHS_{aq} were calculated as follows. The input information included the values of the chemical potential of the complex at various *P-T* conditions (μ_{PT}). The corresponding μ_{PT} values were obtained by processing “raw” experimental data on the solubility values of the solid phases. The solubility was calculated by a modified version of the BALANCE computer program [40], which was designed to simulate equilibria in multicomponent systems. The set of the μ_{PT} values thus obtained was then utilized to calculate the HKF parameters of the AgHS_{aq} complex by the AgHS_{aq} program [27]. The calculation results are summarized in Table 4. The calculated value of the entropy of AgHS_{aq} (34.77 cal mol⁻¹ K⁻¹) is close to the estimate obtained with the use of the ion association model [41] (33–39 cal mol⁻¹ K⁻¹). Moreover, the value assumed for the structural entropy component of AgHS_{aq} is close to the linear dependence of the thermodynamic parameter on the number of ligands (Fig. 5). Linear correlations of this type are typical of various complexes of metals [1, 42], and the occurrence of such a correlation also justifies our choice of the thermodynamic parameter value. It should be mentioned that the adoption of the low-temperature data in [6, 35] leads to a significant deviation of the entropy value for AgHS_{aq} from the model predictions ($S = 16.07$ cal mol⁻¹ K⁻¹) at standard state conditions (Fig. 5).

Ag(HS)₂⁻. The thermodynamic properties and HKF parameters of this complex were assumed according to [3] without any changes, although these authors employed other thermodynamic properties for H₂S_{aq}. Inasmuch as

the predominance region of the Ag(HS)₂⁻ complex lies within the field dominated by the HS⁻ species and its thermodynamic properties were calculated using the reaction



the new parameters of the equation of state for H₂S_{aq} do not affect the thermodynamic properties and HKF parameters of Ag(HS)₂⁻.

Au(HS)₂⁻. Analogously we have processed experimental data on the stability constants of another hydrosulfide complex of Au(I), with regard to newly obtained data on its stability, including that at low temperatures (25–150°C) and the thermodynamic properties of Au₂S [5]. The calculation results are presented in Table 3, and the calculated and experimental data for the whole range of temperature (20–500°C) and pressure (1–1000 bar) are compared in Fig. 3b.

Experimental data [43] on the solubility of Au for broad temperature and pressure ranges were not involved in the optimization procedure because these data were later revised in [7]. The value of the volume of the complex under standard conditions $V_{298} = 75.1$ cm³/mol was assumed as the average of the experimental values of $V_{298} = 60 \pm 20$ cm³/mol [43] and $V_{298} = 85.1 \pm 15$ cm³/mol [31].

AuHS_{aq}. In our earlier publication [3], the thermodynamic properties of the first hydrosulfide complex were predicted using experimental data [31, 32] and data of [33] on the solubility of Au_{cr} in sulfide-bearing solutions at

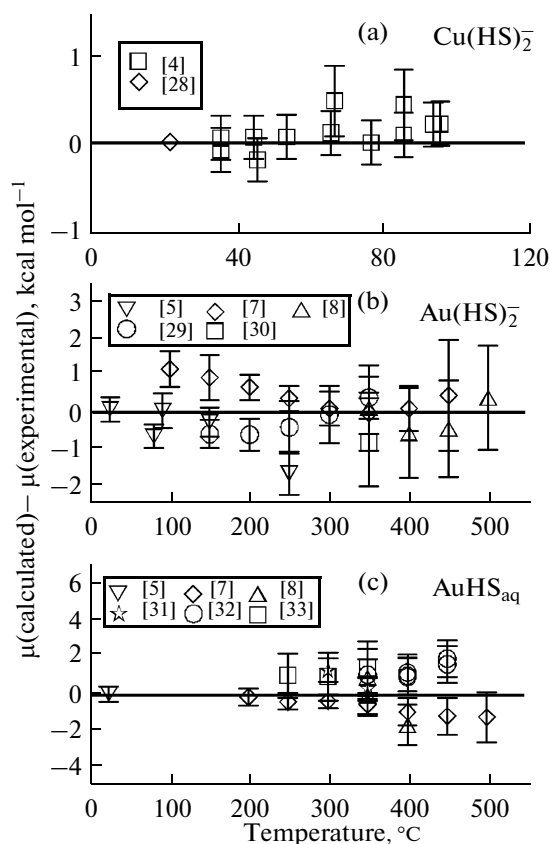


Fig. 3. Temperature dependence of deviations of calculated values of chemical potential μ_{PT} from experimental values for (a) $\text{Cu}(\text{HS})_2^-$, (b) $\text{Au}(\text{HS})_2^-$, and (c) AuHS_{aq} .

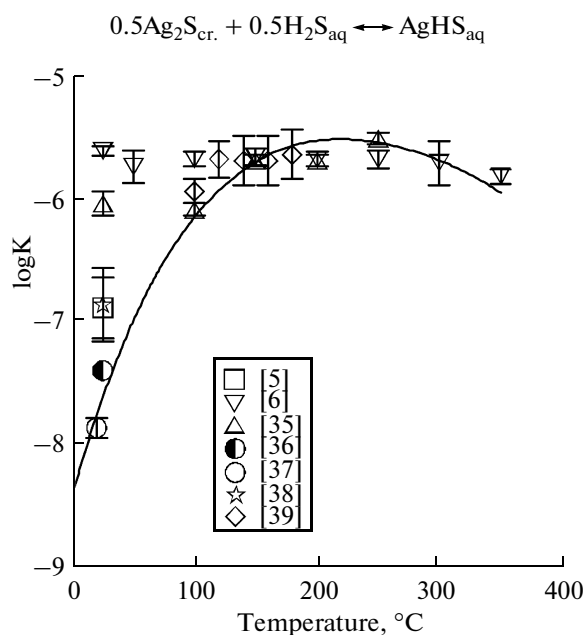


Fig. 4. Temperature dependence of the common logarithm of the constant of the argentite dissolution reaction at water saturation pressure. Symbols—experimental data and line—calculation with the use of parameters for aqueous species of the reaction from Table 3.

temperatures of 250–350°C and water saturation pressure recalculated according to the stoichiometry of the AuHS_{aq} complex. Recently published data [7, 8] cover the ranges of temperature of 200–500°C and pressure of 500–1000 bar, and the Gibbs function for AuHS_{aq} was reliably determined under standard conditions in [5]. All of these experimental data were optimized by the UT-HEL program, to obtain values for $\Delta_f G_{298}^\circ$, S_{298}° , and parameters c_1 and c_2 in the equation for the heat capacity of the complex. The standard values of the heat capacity and volume of AuHS_{aq} were calculated ignoring their changes in the isocoulombic reaction



and using data on AgCl_2^- and AuCl_2^- from [3] and our data on AgHS_{aq} (this publication). Figure 3c illustrates the deviations of the calculated values of the chemical potentials of AuHS_{aq} from the experimental values throughout the whole temperature range. It can be seen that the trends of data [7, 32] with increasing temperature are different. The reasons for this are uncertain.

The internally consistent thermodynamic database presented in this publication for aqueous species in the system Cu–Ag–Au–S–O–H, which involves experimental data published in 2001–2006, makes it possible to simulate geochemical processes in hydrothermal solutions within broad ranges of temperatures (up to 600°C) and pressures (up to 3000 bar).

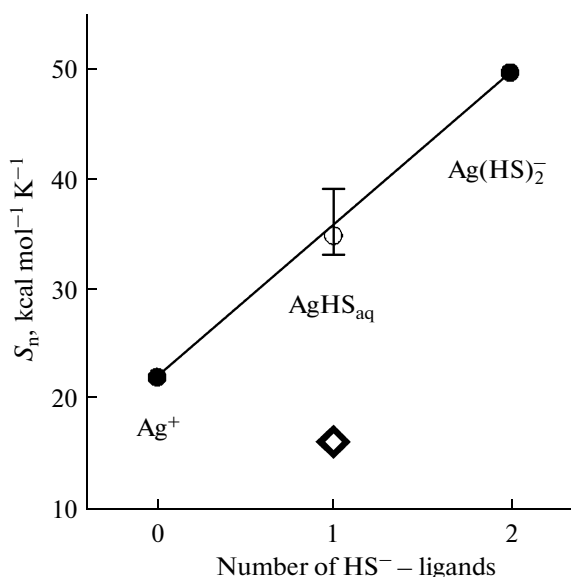


Fig. 5. Dependence of the nonelectrolyte contribution of the entropy of Ag-bearing aqueous species on the number of HS^- ligands under standard conditions. Solid symbols represent reliably determined values of entropy for Ag^+ and $\text{Ag}(\text{HS})_2^-$, from [3], and open circle symbol corresponds to values assumed herein for AgHS_{aq} . Vertical error bars display the prediction by the model of ion association [41], and diamond represents calculations with regard for data in [6, 35].

ACKNOWLEDGMENTS

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